

# A DIFFERENTIAL EVOLUTION APPROACH FOR GLOBAL OPTIMIZATION OF MINLP PROBLEMS

*B.V. Babu\* and Rakesh Angira*

Department of Chemical Engineering  
Birla Institute of Technology & Science  
Pilani - 333 031 (Rajasthan) India

## ABSTRACT

The global optimization of mixed integer non-linear programming (MINLP) problems is an active research area in many engineering fields. In this work, Differential Evolution (DE), a hybrid Evolutionary Computation method, is used for the optimization of nonconvex MINLP problems and a comparison is made among the algorithms based on hybrid of Simplex & Simulated Annealing (M-SIMPASA), Genetic Algorithms (GA), and DE. It is found that DE, an exceptionally simple evolutionary computation method, is significantly faster and yields the global optimum for a wide range of the key parameters. Results indicate that DE is more reliable, efficient and hence a better approach to the optimization of nonconvex non-linear problems. DE found to be the best evolutionary computation method in all the problems studied.

## 1. INTRODUCTION

A large number of process synthesis, design and control problems in Chemical Engineering can be modeled as mixed integer nonlinear programming (MINLP) problems [9, 10, 24]. They involve continuous variables and integers. Due to their combinatorial nature, these problems are considered to be difficult. Gradient optimization techniques have only been able to tackle special formulations, where continuity or convexity had to be imposed, or by exploiting special mathematical structures. Stochastic algorithms, also known as adaptive random search methods, have tackled MINLP problems, mostly in the area of Chemical Engineering [26]. There has been a growing interest in algorithms, which are based on the principle of evolution (survival of the fittest) since two decades. They are referred as Evolutionary Algorithms

\*Corresponding Author: Professor of Chemical Engineering & Head of ET Department, ESD (Workshop), BITS, Pilani-333031.  
E-mail: [bvbabu@bits-pilani.ac.in](mailto:bvbabu@bits-pilani.ac.in); Fax: +91-0159-7644183;  
Phone: +91-0159-7645073 Ext. 205

(EA) or Evolutionary Computation methods (EC methods). In recent years, EAs have been applied to the solution of MINLP problems in many engineering applications. The best-known algorithms in this class include Genetic Algorithms (GA), Evolutionary Programming (EP), Evolution Strategies (ES) and Genetic Programming (GP). Also, there are many hybrid systems, which incorporate various features of the above paradigms and consequently are hard to classify, which can be referred just as EC methods [11]. They differ from the conventional algorithms since, in general, only the information regarding the objective function is required.

Differential Evolution (DE) is one such technique that is exceptionally simple, fast and robust. It is basically a computerized search and optimization algorithm and is more likely to find a function's true global optimum.

So far various methods such as branch and bound technique [18], outer-approximation (OA)/equality-relaxation algorithm [14, 15, 16], variant of OA method [28], adaptive random-search method [26], branch-and-reduce algorithm [17], MINLP Simplex Simulated Annealing Algorithm (M-SIMPASA) [24], and genetic algorithm & evolution strategies [23] have been used for solving MINLP problems. In the present study, seven test problems are studied using DE. These are difficult non-convex optimization problems with continuous and discrete variables. Hence the optimization needs an efficient strategy in searching for the global optimum.

## 2. DIFFERENTIAL EVOLUTION (DE)

DE [21] is an improved version of GA [12] for faster optimization. Unlike simple GA that uses binary coding for representing problem parameters, DE uses real coding of floating point numbers. Among the DE's advantages are its simple structure, ease of use, speed and robustness. Price & Storn [21] gave the working principle of DE with single strategy. Later on, they suggested ten different strategies of DE [22]. A strategy that works out to be the best for a given problem may not work well when applied

for a different problem. Also, the strategy and key parameters to be adopted for a problem are to be determined by trial & error. The key parameters of control are: NP - the population size, CR - the crossover constant, F - the weight applied to random differential (scaling factor). The detailed Differential Evolution algorithm used in the present study is given below:

- Choose a strategy
- Initialize the value of D (Number of independent parameters), NP, CR, F & gen\_max.
- Initialize all the vector population randomly in the given upper & lower bound.  
For I=1 to NP  
{For j=1 to D  
x<sub>ij</sub> = random Number}
- Evaluate the cost of each vector.
- Find out the vector with the lowest cost.
- Repeat
- Perform mutation & recombination.
  - a) For each vector x<sub>i</sub> (target vector), select three distinct vectors x<sub>a</sub>, x<sub>b</sub> & x<sub>c</sub> (select five, if two vector differences are to be used) randomly from the current population (primary array) other than vector x<sub>i</sub>.
  - b) Perform crossover for each target vector with its noisy vector to create a trial vector.
- After the mutation & recombination, if the bound (i.e. lower & upper limit of a variable) is violated then it can be brought in the bound range (i.e. between lower & upper limit) either by forcing it to lower/upper limit (forced bound) or by randomly assigning a value in the bound range (without forcing).
- Perform selection for each target vector, x<sub>i</sub> by comparing its cost with that of the trial vector. Vector with lower cost is selected for next generation.
- Till termination criteria do not meet.
- Print results.

The crucial idea behind DE is a scheme for generating trial parameter vectors. Basically, DE adds the weighted difference between two population vectors to a third vector. Price & Storn [22] have given some simple rules for choosing key parameters of DE for any given application. DE has been successfully applied in various fields. The various applications of DE are: digital filter design [27], batch fermentation process [13, 19], dynamic optimization of continuous polymer reactor [25], estimation of heat transfer parameters in trickle bed reactor [3], optimal design of heat exchangers [7, 8], synthesis & optimization of heat integrated distillation system [6], optimization of an alkylation reaction [1], scenario-integrated optimization of dynamic systems [2], optimization of non-linear functions [4], optimization of thermal cracker operation [5] etc.

### 3. CASE STUDIES

To illustrate the applicability of DE to the nonconvex MINLP problems, seven test problems proposed by different authors are solved. Problem-2 and Problem-4, with equality constraints were difficult to deal with. Hence, the problems are reformulated (as Problem-2\* and Problem-4\*) by eliminating the equality constraints and incorporating them in inequality constraints and/or in objective function thereby reducing the number of constraints and parameters.

**Problem-1:** This example has a non-linear constraint and has been proposed by Kocis & Grossmann [15]. It has also been solved by other authors [9, 17, 23, 24].

$$\text{Min } f(x, y) = 2x + y$$

Subject to

$$1.25 - x^2 - y \leq 0$$

$$x + y \leq 1.6$$

$$0 \leq x \leq 1.6$$

$$y \in \{0, 1\}$$

The global optimum is  $(x, y, f) = (0.5, 1; 2)$ .

**Problem-2:** This problem, with a non-linear constraint is proposed by Kocis & Grossmann [16] and also studied by few other authors [23, 24, 26].

$$\text{Min } f(x_1, x_2, y) = -y + 2x_1 + x_2$$

Subject to

$$x_1 - 2\exp(-x_2) = 0$$

$$-x_1 + x_2 + y \leq 0$$

$$0.5 \leq x_1 \leq 1.4$$

$$y \in \{0, 1\}$$

The global optimum is  $(x_1, x_2, y, f) = (1.375, 0.375, 1; 2.124)$ .

**Problem-2\*:** Problem-2 can be reformulated as follows:

$$\text{Min } f(x_1, y) = -y + 2x_1 - \ln(x_1/2)$$

Subject to

$$-x_1 - \ln(x_1/2) + y \leq 0$$

$$0.5 \leq x_1 \leq 1.4$$

$$y \in \{0, 1\}$$

The global optimum is same as in Problem-2.

**Problem-3:** It presents a non-linear constraint. It was first studied by Floudas [10] and also solved by others [23, 24].

$$\text{Min } f(x_1, x_2, y) = -0.7y + 5(x_1 - 0.5)^2 + 0.8$$

Subject to

$$-\exp(x_1 - 0.2) - x_2 \leq 0$$

$$x_2 + 1.1y \leq -1.0$$

$$\begin{aligned}
x_1 - y &\leq 0.2 \\
0.2 &\leq x_1 \leq 1 \\
-2.22554 &\leq x_2 \leq -1 \\
y &\in \{0, 1\}
\end{aligned}$$

The global optimum is  $(x_1, x_2, y, f) = (0.94194, -2.1, 1, 1.07654)$ .

**Problem-4:** It has been taken from Kocis & Grossmann [14]. The objective here is to select one between two candidate reactors in order to minimize the production cost. Also, it has been solved by others [23, 24, 28, 29].

$$\text{Min } f(x, y_1, y_2, v_1, v_2) = 7.5y_1 + 5.5y_2 + 7v_1 + 6v_2 + 5x$$

Subject to

$$\begin{aligned}
y_1 + y_2 &= 1 \\
z_1 &= 0.9[1 - \exp(-0.5v_1)]x_1 \\
z_2 &= 0.8[1 - \exp(-0.4v_2)]x_2 \\
z_1 + z_2 &= 10 \\
x_1 + x_2 &= x \\
z_1y_1 + z_2y_2 &= 10 \\
v_1 &\leq 10y_1 \\
v_2 &\leq 10y_2 \\
x_1 &\leq 20y_1 \\
x_2 &\leq 20y_2 \\
x_1, x_2, z_1, z_2, v_1, v_2 &\geq 0 \\
y_1, y_2 &\in \{0, 1\}
\end{aligned}$$

The global optimum is:  $(x, y_1, y_2, v_1, v_2; f) = (13.36227, 1, 0, 3.514237, 0, 99.245209)$ .

**Problem-4\*:** This can be reformulated without equality constraints as follows:

$$\begin{aligned}
\text{Min } f(y_1, v_1, v_2) &= 7.5y_1 + 5.5(1 - y_1) + 7v_1 + 6v_2 \\
&+ 50 \frac{1 - y_1}{0.8[1 - \exp(-0.4v_2)]} + 50 \frac{y_1}{0.9[1 - \exp(-0.5v_1)]}
\end{aligned}$$

Subject to

$$\begin{aligned}
0.9[1 - \exp(-0.5v_1)] - 2y_1 &\leq 0 \\
0.8[1 - \exp(-0.4v_2)] - 2(1 - y_1) &\leq 0 \\
v_1 &\leq 10y_1 \\
v_2 &\leq 10(1 - y_1) \\
v_1, v_2 &\geq 0 \\
y_1 &\in \{0, 1\}
\end{aligned}$$

The global optimum is same as in Problem-4.

**Problem-5:** This problem was studied by many authors [9, 17, 23, 24, 26]. It presents several nonlinear constraints.

$$\text{Min } f(x_1, x_2, x_3, y_1, y_2, y_3, y_4) = (y_1 - 1)^2 + (y_2 - 1)^2 + (y_3 - 1)^2 - \ln(y_4 + 1) + (x_1 - 1)^2 + (x_2 - 2)^2 + (x_3 - 3)^2.$$

Subject to

$$\begin{aligned}
y_1 + y_2 + y_3 + x_1 + x_2 + x_3 &\leq 5 \\
y_3^2 + x_1^2 + x_2^2 + x_3^2 &\leq 5.5
\end{aligned}$$

$$\begin{aligned}
y_1 + x_1 &\leq 1.2 \\
y_2 + x_2 &\leq 1.8 \\
y_3 + x_3 &\leq 2.5 \\
y_4 + x_1 &\leq 1.2 \\
y_2^2 + x_2^2 &\leq 1.64 \\
y_3^2 + x_3^2 &\leq 4.25 \\
y_2^2 + x_3^2 &\leq 4.64 \\
x_1, x_2, x_3 &\geq 0 \\
y_1, y_2, y_3, y_4 &\in \{0, 1\}
\end{aligned}$$

The global optimum is  $(x_1, x_2, x_3, y_1, y_2, y_3, y_4; f) = (0.2, 1.28062, 1.95448, 1, 0, 0, 1; 3.557473)$ .

**Problem-6:** It is taken from Wong [20] and also studied by others [23, 24].

$$\text{Max } f(x_1, x_2, x_3, y_1, y_2) = -5.357854x_1^2 - 0.835689y_1x_3 - 37.29329y_1 + 40792.141.$$

Subject to

$$\begin{aligned}
a_1 + a_2y_2x_3 + a_3y_1x_2 - a_4x_1x_3 &\leq 92 \\
a_5 + a_6y_2x_3 + a_7y_1y_2 + a_8x_1^2 - 90 &\leq 20 \\
a_9 + a_{10}x_1x_3 + a_{11}y_1x_1 + a_{12}x_1x_2 - 20 &\leq 5 \\
27 &\leq x_1, x_2, x_3 \leq 45 \\
y_1 &\in \{78, \dots, 102\}, \text{ integer} \\
y_2 &\in \{33, \dots, 45\}, \text{ integer}
\end{aligned}$$

where  $a_1$  to  $a_{12}$  are constants the values of which are given in [23].

The global optimum (for any combination of  $x_2, y_2$ ) is:  $(x_1, x_3, y_1; f) = (27, 27, 78; 32217.4)$ .

**Problem-7:** This is a multi-product batch plant problem with  $M$  serial processing stages, where fixed amounts  $Q_i$  from  $N$  products must be produced. Many authors [15, 18, 23, 24, 26] studied this problem.

$$\text{Min } f = \sum_{j=1}^M \alpha N_j V_j^\beta$$

Subject to

$$\begin{aligned}
\sum_{i=1}^N \frac{Q_i T_{Li}}{B_i} &\leq H \\
V_j &\geq S_{ij} B_i \\
N_j T_{Li} &\geq t_{ij} \\
1 &\leq N_j \leq N_j^u \\
V_j^l &\leq V_j \leq V_j^u \\
T_{Li}^l &\leq T_{Li} \leq T_{Li}^u \\
B_j^l &\leq B_j \leq B_j^u
\end{aligned}$$

where, for the specific problem considered,  $M = 3, N = 2, H = 6000, \alpha_j = 250, \beta_j = 0.6, N_j^u = 3, V_j^l = 250$  and  $V_j^u = 2500$ . The values of  $T_{Li}^l, T_{Li}^u, B_j^l$  and  $B_j^u$  are given by:

$$\begin{aligned}
T_{Li}^l &= \max t_{ij} / N_j^u \\
T_{Li}^u &= \max t_{ij} \\
B_j^l &= Q_i * T_{Li} / H
\end{aligned}$$

$$B_j^u = \min(Q_i, \min_j V_j^u/S_{ij})$$

The values of  $S_{ij}$  and  $t_{ij}$  [ $i = 1$  to 2 (rows); and  $j = 1$  to 3 (columns)] are reported in [23].

The global optimum is:  $(N_1, N_2, N_3, V_1, V_2, V_3, B_1, B_2, T_1, T_2, f) = (1, 1, 1, 480, 720, 960, 240, 120, 20, 16; 38499.8)$ .

#### 4. RESULTS AND DISCUSSION

Table-1 shows the results obtained using DE with/without forcing the bound on variables, and Table-2 presents the comparison of DE with GA & M-SIMPISA. The stopping criteria adopted for DE is to terminate the search process when one of the following conditions is satisfied: (1) the maximum number of generations is reached (assumed 5000 generations for Problem-7 & 1000 generations for other problems). (2)  $|f_{\max}^k - f_{\min}^k| < 10^{-5}$  where  $f$  is the value of objective function for  $k$ -th generation. After the mutation & recombination, if the bound (i.e. lower & upper limit of a variable) is violated then it can be brought in the bound range (i.e. between lower & upper limit) either by forcing it to lower/upper limit (forced bound) or by randomly assigning a value in the bound range (without forcing). In Table-1 & Table-2, NFE & NRC represent respectively, the mean number of objective function evaluations and the percentage of runs converged to the global optimum in all the 10 executions (with different seed values).

In Problem-1 & Problem-2, NFE without forcing is slightly less than NFE with forced bound (Table-1). However, for other problems NFE with forced bound is significantly less than NFE without forcing. Also, the NRC with forced bound is not 100% in problems 2\*, 3, 5 & 7 while NRC without forcing is 100% for all the problems. It is important to note that in Problem-3, NRC with forced bound is zero. It is because when upper limit of bound is violated, the value of variable is forced to the upper limit that resulted in convergence to non-optimal solution. However, for Problem-7, the NRC is 70% for forced bound and 10% without forcing the bound.

Table-2 shows the comparison of DE (without forcing the bound) with GA & M-SIMPISA. The NFE in DE is less than 11% of that in GA for all the problems (The range is 3% to 10.15% to be precise). However, for Problem-7, only DE is converging, while GA and M-SIMPISA are not converging to global optimum. Similarly, the NFE in DE ranges from 3.88% to 66.33 % of that in M-SIMPISA. Therefore, it is evident that DE took least NFE and maximum NRC to achieve global optima in each of the above test problems. It may be noted that GA could not converge to global optimum, while execution was reported to be halted in M-SIMPISA for Problem-7. Hence the performance of DE proved to be better than that of GA & M-SIMPISA in optimizing the mixed integer nonlinear programming problems considered in the present study.

**Table-1. Results of DE<sup>1</sup>**

Problem No.	DE <sup>1</sup> NFE/NRC (Forced bound)	DE <sup>1</sup> NFE/NRC (Without forcing)	Key parameters of DE <sup>1</sup> (NP/CR/F)
1	424/100	402/100	10/0.7/0.5
2*	442/80	410/100	10/0.9/0.7
3	352**/0	4346/100	20/0.8/0.7
4*	580/100	1416/100	20/0.8/0.5
5	9348/80	10425/100	30/0.6/0.9
6	414/100	3542/100	20/0.8/0.5
7	196786/70	222400/10	100/0.8/0.3

DE<sup>1</sup> Strategy used is DE/rand/1/bin (Price and Storn, 2002)

\*\* Converged to a non-optimal solution

NFE = NP (1 + Number of generations)

**Table-2. Comparison of DE<sup>1</sup>, GA & M-SIMPISA**

Problem No.	NFE/NRC (GA)	NFE/NRC (M-SIMPISA)	NFE/NRC (DE <sup>1</sup> )
1	6787/100	607/99	402/100
2*	13939/100	10582/83	410/100
3	107046/90	#/0	4346/100
4*	22489/100	14738/100	1416/100
5	102778/60	22309/60**	10425/100
6	37167/100	27410/87	3542/100
7	225176/0	#/0	222400/10

# Execution halted

#### 5. CONCLUSIONS

Seven chemical engineering case study problems have been solved using DE in the present work. Results indicate that the bound on variables, when violated, should not be forced to lower/upper limit. In such cases, assigning a random value between lower & upper limit found to give 100% convergence to global optimum. Also there was difficulty in dealing with equality constraints (Problem-2 and Problem-4). However, when reformulated by eliminating these equality constraints, the algorithm exhibited 100% convergence. It is found that NFE is the least and NRC is highest in DE as compared to GA & M-SIMPISA. The performance of DE proved to be the best among the three population based methods for all the problems studied.

#### 6. REFERENCES

- [1] B. V. Babu, and Gaurav Chaturvedi, "Evolutionary Computation strategy for Optimization of an Alkylation Reaction", *Proceedings of 53rd Annual Session of IChE (CHEMCON-2000)*, Calcutta, December 18-21, 2000.

- [2] B. V. Babu, and K. Gautam, "Evolutionary Computation for Scenario-Integrated Optimization of Dynamic Systems", *Proceedings of 54th Annual Session of IChE (CHEMCON-2001)*, Chennai, December 19-22, 2001.
- [3] B. V. Babu, and K. K. N. Sastry, "Estimation of heat-transfer parameters in a trickle-bed reactor using differential evolution and orthogonal collocation", *Computers & Chemical Engineering*, 23, 327-339, 1999.
- [4] B. V. Babu, and Rakesh Angira, "Optimization of Non-linear functions using Evolutionary Computation", *Proceedings of 12<sup>th</sup> ISME Conference*, Chennai, India, Jan, 10-12, 153-157, 2001.
- [5] B. V. Babu, and Rakesh Angira, "Optimization of thermal cracker operation using Differential Evolution", *Proceedings of 54th Annual Session of IChE (CHEMCON-2001)*, Chennai, December 19-22, 2001.
- [6] B. V. Babu, and Rishinder Pal Singh, "Synthesis & optimization of Heat Integrated Distillation Systems Using Differential Evolution", *Proceedings of All-India seminar on Chemical Engineering Progress on Resource Development: A Vision 2010 and Beyond*, IE (I), Bhubaneswar, India, March 11, 2000.
- [7] B. V. Babu, and S. A. Munawar, "Differential Evolution for the optimal design of heat exchangers", *Proceedings of All-India seminar on Chemical Engineering Progress on Resource Development: A Vision 2010 and Beyond*, IE (I), Bhubaneswar, India, March 11, 2000.
- [8] B. V. Babu, and S. A. Munawar, "Optimal Design of Shell & Tube Heat Exchanger by Different strategies of Differential Evolution", *PreJournal.com - The Faculty Lounge, Article No. 003873, posted on website Journal <http://www.prejournal.com>*, March 03, 2001.
- [9] C. A. Floudas, A. Aggarwal, and A. R. Ciric, "Global optimum search for nonconvex NLP and MINLP problems", *Computers & Chemical Engineering*, 13 (10), 1117-1132, 1989.
- [10] C. A. Floudas, *Nonlinear and mixed-integer optimization*, Oxford University Press, New York, 1995.
- [11] D. Dasgupta, and Z. Michalewicz, *Evolutionary algorithms in Engineering Applications*, Springer, Germany, 1997.
- [12] D. E. Goldberg, *Genetic algorithms in search, optimization, and machine learning*, Reading, MA: Addison-Wesley, 1989.
- [13] F. S. Wang, and W. M. Cheng, "Simultaneous optimization of feeding rate and operation parameters for fed-batch fermentation processes", *Biotechnology Progress*, 15 (5), 949-952, 1999.
- [14] G. R. Kocis, and I. E. Grossmann, "A modeling and decomposition strategy for the MINLP optimization of process flowsheets", *Computers & Chemical Engineering*, 13, 797-819, 1989.
- [15] G. R. Kocis, and I. E. Grossmann, "Global optimization of nonconvex mixed-integer nonlinear programming (MINLP) problems in process synthesis", *Industrial & Engineering Chemistry Research*, 27, 1407-1421, 1988.
- [16] G. R. Kocis, and I. E. Grossmann, "Relaxation strategy for the structural optimization of process flow sheets", *Industrial & Engineering Chemistry Research*, 26, 1869-1880, 1987.
- [17] H. S. Ryoo, and B. P. Sahinidis, "Global optimization of nonconvex NLPs and MINLPs with application in process design", *Computers & Chemical Engineering*, 19, 551, 1995.
- [18] I. E. Grossmann, and R. W. H. Sargent, "Optimal design of multipurpose chemical plants", *Industrial & Engineering Chemistry Process design development*, 31, 262, 1979.
- [19] J. P. Chiou, and F. S. Wang, "Hybrid method of evolutionary algorithms for static and dynamic optimization problems with application to a fed-batch fermentation process", *Computers & Chemical Engineering*, 23, 1277-1291, 1999.
- [20] J. Wong, "Computational experience with a general nonlinear programming algorithm", *COED J*, 10, 19, 1990.
- [21] K. Price, and R. Storn, "Differential Evolution - A simple evolution strategy for fast optimization", *Dr. Dobb's Journal*, 22 (4), 18-24 and 78, 1997.
- [22] K. Price, and R. Storn, *Web site of DE*, April 2002. URL: <http://www.ICSI.Berkeley.edu/~storn/code.html>
- [23] L. Costa, and P. Olivera, "Evolutionary algorithms approach to the solution of mixed integer no-linear programming problems", *Computers & Chemical Engineering*, 25, 257-266, 2001.
- [24] M. F. Cardoso, R. L. Salcedo, S. Fayo de Azevedo, and D. Barbosa, "A simulated annealing approach to the solution of MINLP problems", *Computers & Chemical Engineering*, 21, 1349-1364, 1997.
- [25] M. H. Lee, C. Han, and K. S. Chang, "Dynamic optimization of a continuous polymer reactor using a modified differential evolution", *Industrial & Engineering Chemistry Research*, 38, 4825-4831, 1999.
- [26] R. L. Salcedo, "Solving nonconvex nonlinear programming problems with adaptive random search", *Industrial & Engineering Chemistry Research*, 31, 262, 1992.
- [27] R. Storn, "Differential Evolution design of an IIR-filter with requirements for magnitude and group delay", *International Computer Science Institute*, TR-95-026, May, 1995.
- [28] U. M. Diwekar, I. E. Grossmann, and E. S. Rubin, "An MINLP Process Synthesizer for a Sequential Modular Simulator", *Industrial & Engineering Chemistry Research*, 31, 313-322, 1992.
- [29] U. M. Diwekar, and E. S. Rubin, "Efficient handling of the implicit constraints problem for the ASPEN MINLP Synthesizer", *Industrial & Engineering Chemistry Research*, 32, 2006-2011, 1993.